

# PHOSPHONIC ACID MODIFICATION TO MOLYBDENUM ATOM CATALYST FOR CO<sub>2</sub> HYDROGENATION ON MAGNESIUM HYDRIDE SURFACE

Gumawa Windu Manggada<sup>1,2</sup> and Shixue Zhou<sup>2</sup>

<sup>1</sup>Department of Chemical Engineering, Politeknik Negeri Malang, Soekarno-Hatta Street No. 9,

Malang 65141, Indonesia

<sup>2</sup>College of Chemical and Biological Engineering, Shandong University of Science and Technology,

579 Qianwangang Road, Qingdao 266590, China

gumawawindu@gmail.com; [zhoushixue66@163.com]

#### ABSTRACT

Catalytic hydrogenation is one of the most effective ways to convert  $CO_2$  to high value-added chemicals, and it is challenging to improve the catalytic activity and product selectivity based on the understanding of catalysis mechanism of the process. In this work, organic phosphonic acid was innovatively employed to tune single atom catalyst for  $CO_2$  hydrogenation to methanol, and the effect of fluoromethylphosphonic acid (FMPA) on the electronic structure of molybdenum and the reaction energy barriers of  $CO_2$  hydrogenation on MgH<sub>2</sub> surface were investigated by density functional theory (DFT) calculations. The results showed that the reaction energy barriers at the key steps were significantly decreased by the introduction of FMPA, which stabilized the reaction intermediates from  $CO_2$  hydrogenation on FMPA/Mo-MgH<sub>2</sub>(001) surface with energy barrier only 1.22 eV at the rate-determining step, and CH<sub>3</sub>OH was the overwhelming product rather than HCOOH, H<sub>2</sub>CO, CO or CH<sub>4</sub> considering the reaction barriers and adsorption energies. The combination of organic phosphonic acid with single atom catalyst can generate the rational design of new catalytic system, which is helpful to control the reaction pathway and product selectivity.

**Keywords:** carbon dioxide conversion, catalytic hydrogenation, magnesium hydride, organic phosphonic acid, single atom catalyst.

# 1. INTRODUCTION

Carbon dioxide can be used for the synthesis of synthesized into high value-added chemicals as a promising route to reduce greenhouse gas emissions and expand syngas resources [1-3]. Among the various approaches, thermo-catalytic hydrogenation technology is received significant attention [4-6]. Although many studies on CO<sub>2</sub> hydrogenation have been conducted, controlling product selectivity is still challenging.

The yield and selectivity of a product from  $CO_2$  hydrogenation are determined by the reaction pathway. There are two possible reaction pathways, the formate pathway and the reverse water gas shift (RWGS) pathway, for  $CO_2$  hydrogenation in terms of the first

hydrogenation step of  $CO_2$  to form  $HCOO^*$  or  $COOH^*$  [7, 8]. In the formate pathway, the reaction begins with a H atom approaching the C atom of  $CO_2$  molecule through the formation of formate (HCOO<sup>\*</sup>), followed by intermediate products formic acid (HCOOH) and formaldehyde (H<sub>2</sub>CO) then final product methanol (CH<sub>3</sub>OH) or methane (CH<sub>4</sub>) [9-12]. The RWGS begins with a H atom approaching the O atom of  $CO_2$  and involves the production of carbon monoxide (CO), and then goes on further hydrogenation [13-15].

Magnesium hydride is a prospected candidate for hydrogen storage, and it can be employed for hydrogenation, due to its abundant resources, low cost, and adjustable hydrogen releasing temperature [2, 16-19]. In this work, MgH<sub>2</sub> was used as hydrogen source for hydrogenation by directly providing active H atom from crystal lattice, instead of highpressure hydrogen gas. On the other hand, efficient catalysts are necessary to reduce the activation energy of the stable C=O bonds in CO<sub>2</sub> [12, 20]. Single-atom catalyst (SAC) has attracted much research interest due to its high activity and efficiency [21-23]. In addition, phosphonic acid was reported for the catalysis of methanol conversion [24] and olefin production [25].

This work innovatively aimed to investigate the application of molybdenum single atom catalyst modified with organic phosphonic acid for  $CO_2$  hydrogenation on MgH<sub>2</sub> surface using density functional theory (DFT) calculations. The adsorption of the reaction intermediates and the energy barrier of each elementary step involved in the  $CO_2$ hydrogenation were calculated so that the minimum energy pathway (MEP) was determined. The clarification of the underlying function mechanism in the catalytic activity and product selectivity of  $CO_2$  hydrogenation helps the rational design of an efficient catalytic system.

# 2. COMPUTATIONAL METHOD

The DFT calculations were performed using program package DMol<sup>3</sup> of software Materials Studio (Accelrys Software Inc.). The Perdew-Burke-Ernzerhof (PBE) functional of the generalized gradient approximation (GGA) was employed for the nonlocal exchange and correlation functional, and the electron wave function was based on double numerical plus polarization (DNP) to expand the valence electron function into numerical orbital for calculation accuracy [26]. DFT Semi-core pseudopotential was employed for the core treatment of electrons which represent core electrons by a single effective potential. The computational parameters were tolerance  $1 \times 10^{-6}$  Ha/atom for self-consistent field (SCF) and thermal smearing 0.01 Ha for quick convergence of orbital occupation, and energy tolerance  $1.0 \times 10^{-5}$  Ha/atom, maximum force gradient 0.002 Ha/Å, and maximum atomic displacement 0.005 Å for structure optimization.

The MgH<sub>2</sub>(001) surface was constructed by a periodic three atomic layers of (3×3) unit cell slab with totally 27 Mg and 54 H atoms and separated by a vacuum gap of 20 Å to avoid periodic boundary interactions in all cases (Figure 1a), in which it was verified that the relativity of properties and reaction energy barriers calculated from three atomic layers was consistent with seven atomic layers. The bottom two atom layers were fixed to represent the optimized bulk positions, while others were allowed to relax together with an adsorbate. Brillouin-zone integrations were performed on a grid of  $8 \times 8 \times 12$  Monkhorst-Pack

k-mesh for unit cell optimization, and  $2 \times 2 \times 1$  for supercells. An Mo atom catalyst was loaded on the MgH<sub>2</sub>(001) surface by replacing a Mg atom on the first layer, and fluoromethylphosphonic acid (FMPA) was introduced on the surface to complete the construction of substrate as shown in Figure 1b.



Figure 1. Structural models of (a) MgH<sub>2</sub>(001) supercell and (b) substrate with Mo and FMPA.

The adsorption energy ( $E_{ads}$ ) was calculated as follows:

 $E_{ads} = E_{adsorbate+substrate} - (E_{adsorbate} + E_{substrate})$ (1)

where  $E_{adsorbate+substrate}$ ,  $E_{adsorbate}$ , and  $E_{substrate}$ , are the total energy of the substrate covered with adsorbate, adsorbate, and bare substrate, respectively [11, 27, 28].

The complete LST/QST (linear synchronous transit and quadratic synchronous transit) method was applied to identify the transition state configurations and to calculate relevant energy barriers of elementary steps involved in  $CO_2$  hydrogenation reaction. The energy barrier ( $E_b$ ) and the reaction energy ( $\Delta E$ ) were defined as below:

$$E_{\rm b} = E_{\rm TS} - E_{\rm IS} \tag{2}$$

$$\Delta E = E_{\rm FS} - E_{\rm IS} \tag{3}$$

where  $E_{TS}$ ,  $E_{IS}$ , and  $E_{FS}$  are the total energy of the transition state (TS), initial state (IS), and final state (FS), respectively [11].

# 3. RESULTS AND DISCUSSION

# 3.1 Effect of molybdenum atom and phosphonic acid on $\mbox{CO}_2$ adsorption and primary hydrogenation reactions

The stable adsorption configurations of  $CO_2$  molecule on clean MgH<sub>2</sub>(001) surface and the surfaces with Mo atom and FMPA were shown in Figure 2. On clean MgH<sub>2</sub>(001) surface,  $CO_2$  molecule was far away from the surface. In contrast, on Mo-MgH<sub>2</sub>(001) and FMPA/Mo-MgH<sub>2</sub>(001) surfaces,  $CO_2$  molecule combined with Mo atom to form C-Mo and O-Mo bonds. The adsorption energies of  $CO_2$ , intermediates  $COOH^*$ , CO, and  $HCO^*$  on different surfaces were listed in Table 1. High adsorption energies on Mo-MgH<sub>2</sub>(001) and FMPA/Mo-MgH<sub>2</sub>(001) surfaces were considered capable of weakening chemical bonds of the adsorbates so that the reaction energy barriers became lower.



**Figure 2.** Optimized structures of CO<sub>2</sub> adsorption on MgH<sub>2</sub>(001), Mo-MgH<sub>2</sub>(001) and FMPA/Mo-MgH<sub>2</sub>(001) surfaces

**Table 1.** Adsorption energies of key adsorbates in  $CO_2$  hydrogenation on MgH<sub>2</sub>(001), Mo-MgH<sub>2</sub>(001) and FMPA/Mo-MgH<sub>2</sub>(001) surfaces.

Adcorbato		E <sub>ads</sub> on surface (e	V)
Ausorbate	MgH <sub>2</sub> (001)	Mo-MgH <sub>2</sub> (001)	FMPA/Mo-MgH <sub>2</sub> (001)
CO <sub>2</sub>	-0.09	-3.22	-2.38
COOH <sup>*</sup>	-1.13	-3.58	-4.56
СО	-0.57	-3.14	-3.22
HCO <sup>*</sup>	-0.98	-5.48	-5.30

The energy barriers of key hydrogenation reaction steps on different surfaces were listed in

**Table 2.** Some elementary steps were hindered by high energy barriers, such as  $COOH^*$  formation and dissociation on MgH<sub>2</sub>(001) surface and HCO<sup>\*</sup> formation on Mo-MgH<sub>2</sub>(001) surface, and the introduction of phosphonic acid reduced the reaction energy barriers.

Table 2	. Energy barriers of elementary steps for $CO_2$ hydrogenatic	on on MgH <sub>2</sub> (001), Mo-
	MgH <sub>2</sub> (001) and FMPA/Mo-MgH <sub>2</sub> (001) surfaces.	

		E <sub>b</sub> on surface (eV)	
Adsorbate	MgH <sub>2</sub> (001)	Mo-MgH <sub>2</sub> (001)	FMPA/Mo-MgH <sub>2</sub> (001)
$CO_2 + H^* \rightarrow COOH^*$	1.44	1.05	0.98
$\text{COOH}^* \rightarrow \text{CO+OH}^*$	1.62	0.73	0.66
$CO+H^* \rightarrow HCO^*$	1.04	1.92	1.22

The catalysis of Mo and phosphonic acid was clarified by the deformation charge density distribution and Mulliken atomic charge and the partial density of states (PDOS) analysis of intermediate COOH<sup>\*</sup> on FMPA/Mo-MgH<sub>2</sub>(001) surface compared with clean MgH<sub>2</sub>(001) surface (Figure 3). On FMPA/Mo-MgH<sub>2</sub>(001) surface, Mo atom provided electron density to the antibonding orbital of intermediate COOH<sup>\*</sup> and accepted electron density from the bonding orbital of COOH<sup>\*</sup> simultaneously as shown in Figure 3 (c).

Strong hybridization was found between C atom of intermediate COOH<sup>\*</sup> (C 2s, 2p) and Mo 4d orbital at -2.55 eV on the left of Fermi level and 1.12 eV on the right of Fermi level. It is indicated as the bonding-antibonding pair and referred to the strong chemisorption, as shown in Figure 3 (d), which is in line with the theoretical study in reference [29]. Whereas, the interaction between COOH<sup>\*</sup> and clean MgH<sub>2</sub>(001) surface was weak, as shown in Figure 3 (a) and (b).



**Figure 3.** Deformation charge density and Mulliken atomic charge distribution (a and c) and PDOS profile (b and d) of COOH\* on clean MgH<sub>2</sub>(001) surface and FMPA/Mo-MgH<sub>2</sub>(001) surface.

# 3.2 Reaction Pathway on FMPA/Mo-MgH<sub>2</sub>(001) surface

Two possible reaction pathways, including RWGS and formate pathway for  $CO_2$  hydrogenation, have been considered in this work to further understand the catalytic performance of FMPA/Mo-MgH<sub>2</sub>(001) system and identify the rate-determining step (RDS), in which the pathway had a lower energy barrier of RDS. The overall reaction network is illustrated in Figure 4.



Figure 4. Reaction network and energy barriers for  $CO_2$  hydrogenation on FMPA/Mo-MgH<sub>2</sub>(001) surface. The asterisk (\*) denotes uncoupled electron.

#### 3.2.1 RWGS pathway on FMPA/Mo-MgH<sub>2</sub>(001) surface

At the beginning of RWGS pathway (Figure 4), a H atom bound to the C atom of CO<sub>2</sub> to form COOH<sup>\*</sup> with an energy barrier of 0.98 eV and exothermic energy of -1.94 eV. There were two possible routes for COOH<sup>\*</sup> further reaction. It could be hydrogenated to the C atom to form HCOOH (R4) and further hydrogenated following the formate pathway. Unfortunately, the reaction was hindered by high energy barrier of 3.75 eV. So, the other route in which the dissociation of COOH<sup>\*</sup> into CO with energy barrier only 0.66 eV was preferred. The hydrogenation of CO intermediate to form CH<sub>3</sub>OH could be approached in four different ways. First, the hydrogenation of CO was initiated by the formation of O-H bond to form COH<sup>\*</sup>, then COH<sup>\*</sup> was hydrogenated to form HCOH<sup>\*\*</sup>, H<sub>2</sub>COH<sup>\*</sup>, and CH<sub>3</sub>OH (R7-R13-R20-R24). Second, a H atom was attracted by C atom to form  $HCO^*$ , then followed the same route as in the first way to  $CH_3OH$  (R8-R13-R20-R24). Two other ways were both hydrogenation from CO to produce HCO<sup>\*</sup> then intermediate  $H_2CO$ ; one of which was followed by the formation of an H-O bond to form  $H_2COH^*$  and then CH<sub>3</sub>OH (R8-R15-R21-R24), and another was followed by H-C bond formation to form H<sub>3</sub>CO<sup>\*</sup> and CH<sub>3</sub>OH (R8-R15-R22-R25). The energy barriers of rate-determining step in the four different ways were 2.88, 1.22, 1.83, and 1.39 eV, respectively. Thus, the second route through HCO<sup>\*</sup> and HCOH<sup>\*\*</sup> was the most favorable for the formation of CH<sub>3</sub>OH.

Based on the reaction network, methane was the full hydrogenation product of  $CO_2$  through the hydrogenation of intermediate  $H_3C^*$  with energy barrier of 1.51 eV (R29). For the formation of  $H_3C^*$ , three possible routes were considered. The first route was obtained from the dissociation of  $H_2COH^*$  to  $H_2C^{**}$  and  $OH^*$  and followed by  $H_2C^{**}$  hydrogenation to  $H_3C^*$  (R23-R26), which was hampered by energy barrier of 1.19 eV at the rate-determining step. The second route was generated by the C-OH bond breakup of CH<sub>3</sub>OH with an energy barrier of 2.61 eV (R27). The third possible route was hindered by

the high barrier of 5.41 eV from  $H_3CO^*$  hydrogenation and dissociation to produce  $H_3C^*$  and  $OH^*$ .

Comparing with  $CH_4$  production, methanol was more readily produced from the hydrogenation of  $CO_2$  on FMPA/Mo-MgH<sub>2</sub>(001) surface via RWGS pathway according to the RDS analysis. The minimum energy path of RWGS pathway from  $CO_2$  to  $CH_3OH$  on FMPA/Mo-MgH<sub>2</sub>(001) surface was shown in Figure 5. The rate-determining step was the HCO<sup>\*</sup> formation, which is consistent with the calculation result in reference [30], whereas the energy barrier was much lower, 1.22 eV here versus 1.50 eV on Pd/TiO<sub>2</sub>.



Reaction coordinate

**Figure 5.** Minimum energy path of RWGS pathway for CO<sub>2</sub> hydrogenation on FMPA/Mo-MgH<sub>2</sub>(001) surface.

#### 3.2.2 Formate pathway on FMPA/Mo-MgH<sub>2</sub>(001) surface

Formate pathway was characterized by the formation of intermediate formate  $(HCOO^*)$ . On FMPA/Mo-MgH<sub>2</sub>(001) surface, HCOO<sup>\*</sup> was produced by the hydrogenation of CO<sub>2</sub> when a H attacked the C atom of CO<sub>2</sub> to form a C-H bond (R2) with an energy barrier of 0.79 eV and exothermic energy of -2.80 eV. The possible routes for HCOO<sup>\*</sup> further hydrogenation had 1.72 eV energy barrier at rate-determining step. Therefore, in comparison with RWGS pathway on FMPA/Mo-MgH<sub>2</sub>(001) surface, formate pathway was not favorable to the production of CH<sub>3</sub>OH, which is consistent with the calculation result on Rh-doped Cu(111) surface in reference [31].

# 3.3 Rate-determining steps of $CO_2$ hydrogenation for different $C_1$ products on FMPA/Mo-MgH<sub>2</sub>(001) surface

The adsorption energies, rate-determining steps, energy barriers, and reaction energies of  $C_1$  products from  $CO_2$  hydrogenation on FMPA/Mo-MgH<sub>2</sub>(001) surface were summarized in

Table 3. Through RWGS pathway, the energy barrier of RDS for  $CO_2$  to CO was only 0.98 eV, but the releasing of CO was hindered by high adsorption energy of CO. The further hydrogenation of CO was easy to produce methanol with energy barrier of 1.22

eV. For methane formation, the energy that was needed to overcome the barrier was more than 1.83 eV. On the other hand, the energy barrier of RDS via formate pathway to form formic acid, formaldehyde, and methanol was 1.72, 1.30, and 1.39 eV, respectively. Therefore, methanol was preferred as the main C<sub>1</sub> product of CO<sub>2</sub> hydrogenation on FMPA/Mo-MgH<sub>2</sub>(001) surface.

Product	E <sub>ads</sub> (eV)	Reaction Rate-determining step		E <sub>b</sub> (eV)	Δ <i>Ε</i> (eV)		
СО	-3.22	$CO_2 \rightarrow CO$	$CO_2 + H^* \rightarrow COOH^*$	0.98	-1.93		
нсоон	-0.97	$CO_2 \rightarrow HCOOH$	HCOO <sup>*</sup> +H <sup>*</sup> → HCOOH	1.72	-0.75		
H <sub>2</sub> CO	-3.77	$CO \rightarrow H_2CO$	$HCO^* + H^* \rightarrow H_2CO$	1.24	-1.93		
		$\rm HCOOH \rightarrow \rm H_{2}CO$	$H_2COOH^* + H^* \rightarrow H_2C(OH)_2$	1.30	-1.39		
CH₃OH	-1.38	$CO \rightarrow CH_3OH$	$\text{CO+H}^* \rightarrow \text{HCO}^*$	1.22	-2.14		
		$H_2CO \rightarrow CH_3OH$	$H_3CO^* + H^* \rightarrow CH_3OH$	1.39	-1.19		
$CH_4$	-0.38	$\mathrm{CO} \rightarrow \mathrm{CH}_4$	$H_3C^*+H^* \rightarrow CH_4$	1.51	-1.76		
		$CH_3OH \rightarrow CH_4$	$CH_3OH \rightarrow H_3C^* + OH^*$	2.61	-0.01		
		$\rm H_2CO \rightarrow CH_4$	$H_2CO+H^* \rightarrow H_2COH^*$	1.83	-1.13		

Table	3.	Adsorption	energies,	rate-determining	steps,	and	activation	energies	of	$C_1$
		products from CO <sub>2</sub> hydrogenation on FMPA/Mo-MgH <sub>2</sub> (001) surface.								

# 4. CONCLUSION AND SUGGESTIONS

The introduction of organic phosphonic acid to molybdenum single atom catalyst on  $MgH_2$  surface for  $CO_2$  hydrogenation effectively lowered the reaction energy barriers. Organic phosphonic acid decreased the electron density at molybdenum atom adsorption site and enhanced the stability of reaction intermediates and transition states in  $CO_2$  hydrogenation, and therefore it decreased the reaction energy barriers. On FMPA/Mo-MgH<sub>2</sub>(001) surface, the RWGS pathway was superior to formate pathway with high selectivity of methanol as the C<sub>1</sub> product for  $CO_2$  hydrogenation.

This study will inspire the design of new catalytic system in single atom catalyst by tuning the electron structure with organic phosphonic acid to decrease the reaction energy barrier and improve product selectivity. However, both the selection of a transition metal atom and the functional group of organic phosphonic acid should be optimized for a specific reaction product.

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# REFERENCES

[1] Y. Zheng, W. Zhang, Y. Li, J. Chen, B. Yu, J. Wang, L. Zhang, J. Zhang, Energy related CO<sub>2</sub> conversion and utilization: Advanced materials/nanomaterials, reaction mechanisms and technologies, *Nano Energy*, 40, 512-539, 2017.

- [2] H. Chen, P. Liu, J. Liu, X. Feng, S. Zhou, Mechanochemical in-situ incorporation of Ni on MgO/MgH<sub>2</sub> surface for the selective O-/C-terminal catalytic hydrogenation of CO<sub>2</sub> to CH<sub>4</sub>, *Journal of Catalysis*, 394, 397-405, 2020.
- [3] T.R. Anderson, E. Hawkins, P.D. Jones, CO<sub>2</sub>, the greenhouse effect and global warming: from the pioneering work of Arrhenius and Callendar to today's Earth System Models, *Endeavour*, 40, 178-187, 2016.
- [4] M. Aresta, A. Dibenedetto, A. Angelini, Catalysis for the valorization of exhaust carbon: from CO<sub>2</sub> to chemicals, materials, and fuels. Technological use of CO<sub>2</sub>, *Chemical Reviews*, 114, 1709-1742, 2014.
- [5] Q. Pan, J. Peng, S. Wang, S. Wang, In situ FTIR spectroscopic study of the CO<sub>2</sub> methanation mechanism on Ni/Ce<sub>0.5</sub>Zr<sub>0.5</sub>O<sub>2</sub>, *Catalysis Science & Technology*, 4, 502-509, 2014.
- P.A.U. Aldana, F. Ocampo, K. Kobl, B. Louis, F. Thibault-Starzyk, M. Daturi, P. Bazin, S. Thomas, A.C. Roger, Catalytic CO<sub>2</sub> valorization into CH<sub>4</sub> on Ni-based ceria-zirconia. Reaction mechanism by operando IR spectroscopy, *Catalysis Today*, 215, 201-207, 2013.
- [7] Y. Yang, J. Evans, J.A. Rodriguez, M.G. White, P. Liu, Fundamental studies of methanol synthesis from CO<sub>2</sub> hydrogenation on Cu(111), Cu clusters, and Cu/ZnO(0001), *Physical Chemistry Chemical Physics*, 12, 9909-9917, 2010.
- [8] S. Kattel, P. Ramírez, J. Chen, J. Rodriguez, P. Liu, Active sites for CO<sub>2</sub> hydrogenation to methanol on Cu/ZnO catalysts, *Science*, 355, 1296-1299, 2017.
- [9] J. Ye, C. Liu, D. Mei, Q. Ge, Active oxygen vacancy site for methanol synthesis from CO<sub>2</sub> Hydrogenation on In<sub>2</sub>O<sub>3</sub>(110): A DFT Study, *ACS Catalysis*, 3, 1296-1306, 2013.
- [10] Y.-F. Zhao, R. Rousseau, J. Li, D. Mei, Theoretical study of syngas hydrogenation to methanol on the polar Zn-terminated ZnO(0001) surface, *The Journal of Physical Chemistry C*, 116, 15952-15961, 2012.
- [11] L. Liu, X. Su, H. Zhang, N. Gao, F. Xue, Y. Ma, Z. Jiang, T. Fang, Zirconia-modified copper catalyst for CO<sub>2</sub> conversion to methanol from DFT study, *Applied Surface Science*, 528, 146900, 2020.
- [12] Z. Ou, C. Qin, J. Niu, L. Zhang, J. Ran, A comprehensive DFT study of CO<sub>2</sub> catalytic conversion by H<sub>2</sub> over Pt-doped Ni catalysts, *International Journal of Hydrogen Energy*, 44, 819-834, 2019.
- [13] A.G. Kharaji, A. Shariati, M.A. Takassi, A novel γ-alumina supported Fe-Mo bimetallic catalyst for reverse water gas shift reaction, *Chinese Journal of Chemical Engineering*, 21, 1007-1014, 2013.
- [14] L. Wang, S. Zhang, Y. Liu, Reverse water gas shift reaction over Co-precipitated Ni-CeO<sub>2</sub> catalysts, *Journal of Rare Earths*, 26, 66-70, 2008.
- [15] W. Wang, Y. Zhang, Z. Wang, J.-M. Yan, Q. Ge, C.-J. Liu, Reverse water gas shift over In<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> catalysts, *Catalysis Today*, 259, 402-408, 2016.
- [16] S. Zhou, Q. Zhang, H. Chen, X. Zang, X. Zhou, R. Wang, X. Jiang, B. Yang, R. Jiang, Crystalline structure, energy calculation, and dehydriding thermodynamics of magnesium hydride from reactive milling, *International Journal of Hydrogen Energy*, 40, 11484-11490, 2015.

- [17] H. Chen, N. Ma, J. Li, Y. Wang, C. She, Y. Zhang, X. Li, J. Liu, X. Feng, S. Zhou, Effect of atomic iron on hydriding reaction of magnesium: Atomic-substitution and atomicadsorption cases from a density functional theory study, *Applied Surface Science*, 504, 144489, 2020.
- [18] H. Chen, Z. Han, X. Feng, P. Liu, J. Liu, G. Liu, W. Yuan, T. Ren, S. Zhou, Solid-phase hydrogen in a magnesium-carbon composite for efficient hydrogenation of carbon disulfide, *Journal of Materials Chemistry A*, 6, 3055-3062, 2018.
- [19] P. Selvam, B. Viswanathan, C.S. Swamy, V. Srinivasan, Magnesium and magnesium alloy hydrides, *International Journal of Hydrogen Energy*, 11, 169-192, 1986.
- [20] H. Chen, P. Liu, J. Li, Y. Wang, C. She, J. Liu, L. Zhang, Q. Yang, S. Zhou, X. Feng, MgH<sub>2</sub>/Cu<sub>x</sub>O Hydrogen storage composite with defect-rich surfaces for carbon dioxide hydrogenation, ACS Applied Materials & Interfaces, 11, 31009-31017, 2019.
- [21] N. Cheng, L. Zhang, K. Doyle-Davis, X. Sun, Single-atom catalysts: from design to application, *Electrochemical Energy Reviews*, 2, 539-573, 2019.
- [22] A.L. Maulana, R.I.D. Putra, A.G. Saputro, M.K. Agusta, Nugraha, H.K. Dipojono, DFT and microkinetic investigation of methanol synthesis via CO<sub>2</sub> hydrogenation on Ni(111)-based surfaces, *Physical Chemistry Chemical Physics*, 21, 20276-20286, 2019.
- [23] C.-M. Wang, Y.-D. Wang, J.-W. Ge, Z.-K. Xie, Reaction: industrial perspective on single-atom catalysis, *Chem*, 5, 2736-2737, 2019.
- [24] S. Okazaki, M. Kurimata, T. Iizuka, K. Tanabe, The effect of phosphoric acid treatment on the catalytic property of niobic acid, *Bulletin of the Chemical Society of Japan*, 60, 37-41, 1987.
- [25] J. William S. Wadsworth, Synthetic applications of phosphoryl-stabilized anions, *Organic Reactions*, 25, 77-145, 1977.
- [26] B. Delley, From molecules to solids with the DMol<sup>3</sup> approach, *The Journal of Chemical Physics*, 113, 7756-7764, 2000.
- [27] M. Huš, V.D.B.C Dasireddy, N. Strah Štefančič, B. Likozar, Mechanism, kinetics, and thermodynamics of carbon dioxide hydrogenation to methanol on Cu/ZnAl<sub>2</sub>O<sub>4</sub> spinel-type heterogeneous catalysts, *Applied Catalysis B: Environmental*, 207, 267-278, 2017.
- [28] H. Chen, M. Yang, J. Liu, G. Lu, X. Feng, Insight into the effects of electronegativity on the H<sub>2</sub> catalytic activation for CO<sub>2</sub> hydrogenation: four transition metal cases from a DFT study, *Catalysis Science & Technology*, 10, 5641-5647, 2020.
- [29] B. Hammer, J.K. Nørskov, Theoretical surface science and catalysis—Calculations and concepts, *Advances in Catalysis*, 25, 71-129, 2000.
- [30] Z. Ou, J. Ran, J. Niu, C. Qin, W. He, L. Yang, A density functional theory study of CO<sub>2</sub> hydrogenation to methanol over Pd/TiO<sub>2</sub> catalyst: The role of interfacial site, *International Journal of Hydrogen Energy*, 45, 6328-6340, 2020.
- [31] L. Liu, F. Fan, M. Bai, F. Xue, X. Ma, Z. Jiang, T. Fang, Mechanistic study of methanol synthesis from CO<sub>2</sub> hydrogenation on Rh-doped Cu(111) surfaces, *Molecular Catalysis*, 466, 26-36, 2019.